

**HRK 24.6**
**24.6 (a)**

First calculate the pressure in standard units

$$P = \frac{1.1 \times 10^{-7} \text{ cm Hg}}{76 \text{ cm Hg}} (1.01 \times 10^5 \text{ Pa}) = 1.46 \times 10^{-4} \text{ Pa}$$

The ‘number density’  $\rho_n$  is given by

$$\begin{aligned} \rho_n &= \frac{N}{V} = \frac{P}{kT} \\ &= \frac{1.46 \times 10^{-4}}{(1.38 \times 10^{-23})(295)} \\ &= 3.59 \times 10^{16} \text{ molecules/m}^3 \end{aligned}$$

**24.6 (b)**

$$\begin{aligned} \lambda &= \frac{1}{\sqrt{2} \pi \rho_n d^2} \\ \lambda &= \frac{1}{\sqrt{2} \pi (3.59 \times 10^{16})(2.2 \times 10^{-10})^2} \\ \lambda &= 129.5 \text{ m} \end{aligned}$$

**HRK 24.24**

We use the Maxwell-Boltzmann energy distribution

$$n(E) = \frac{2N}{\sqrt{\pi} (kT)^{\frac{3}{2}}} E^{\frac{1}{2}} e^{-\frac{E}{kT}}$$

and the fraction of particles with energy between  $.01 kT$  and  $.03 kT$  is

$$\begin{aligned} \text{fraction} &= \frac{1}{N} \int_{.01kT}^{.03kT} n(E) dE \\ \text{fraction} &= \frac{2}{\sqrt{\pi} (kT)^{\frac{3}{2}}} \int_{.01kT}^{.03kT} E^{\frac{1}{2}} e^{-\frac{E}{kT}} dE \\ \text{fraction} &\approx \frac{2}{\sqrt{\pi} (kT)^{\frac{3}{2}}} \int_{.01kT}^{.03kT} E^{\frac{1}{2}} \left(1 - \frac{E}{kT}\right) dE \\ \text{fraction} &\approx \frac{2}{\sqrt{\pi} (kT)^{\frac{3}{2}}} \int_{.01kT}^{.03kT} E^{\frac{1}{2}} - \frac{E^{\frac{3}{2}}}{kT} dE \\ \text{fraction} &\approx \frac{2}{\sqrt{\pi} (kT)^{\frac{3}{2}}} \left[ \frac{2E^{\frac{3}{2}}}{3} - \frac{2E^{\frac{5}{2}}}{5kT} \right]_{.01kT}^{.03kT} \\ \text{fraction} &\approx \frac{2}{\sqrt{\pi} (kT)^{\frac{3}{2}}} \left[ \left( \frac{2(.03kT)^{\frac{3}{2}}}{3} - \frac{2(.03kT)^{\frac{5}{2}}}{5kT} \right) \right. \\ &\quad \left. - \left( \frac{2(.01kT)^{\frac{3}{2}}}{3} - \frac{2(.01kT)^{\frac{5}{2}}}{5kT} \right) \right] \\ \text{fraction} &\approx \frac{2}{\sqrt{\pi}} \left[ \left( \frac{2(.03)^{\frac{3}{2}}}{3} - \frac{2(.03)^{\frac{5}{2}}}{5} \right) \right. \\ &\quad \left. - \left( \frac{2(.01)^{\frac{3}{2}}}{3} - \frac{2(.01)^{\frac{5}{2}}}{5} \right) \right] \\ \text{fraction} &\approx 0.0031 \quad \text{i.e. } 31\% \end{aligned}$$

**HRK 24.31**

We have 6 degrees of freedom, 3 translational and 3 rotational.

**24.31 (a)**

$$\begin{aligned} E_{trans} = \frac{1}{2}m\langle v_x^2 + v_y^2 + v_z^2 \rangle &= \frac{3}{2}k_B T \\ \langle \frac{1}{2}mv^2 \rangle &= \frac{3}{2}k_B T \\ \Rightarrow \langle v^2 \rangle &= \frac{3k_B T}{m} \end{aligned}$$

$$\begin{aligned} \text{Now use: } m &= \rho V = \frac{4}{3}\pi r^3 \rho \\ m &= 3.35 \times 10^{-20} \text{ kg} \end{aligned}$$

$$\begin{aligned} \text{so that } \langle v^2 \rangle &= \frac{3(1.38 \times 10^{-23})(100)}{3.35 \times 10^{-20}} \\ \langle v^2 \rangle &= 0.12354 \\ \Rightarrow v_{rms} &= \sqrt{\langle v^2 \rangle} = 0.3515 \text{ m/s} \end{aligned}$$

**24.31 (b)**

Because this shape has non-zero length in all 3 dimensions, we have contributions to the rotational energy from rotations about all three axes

$$\begin{aligned} E_{rot} = \frac{1}{2}I\langle \omega_x^2 + \omega_y^2 + \omega_z^2 \rangle &= \frac{3}{2}k_B T \\ \langle \frac{1}{2}I\omega^2 \rangle &= \frac{3}{2}k_B T \\ \Rightarrow \langle \omega^2 \rangle &= \frac{3k_B T}{I} \\ \langle \omega^2 \rangle &= \frac{(3)(5)k_B T}{2mr^2} \quad \text{using } I_{sphere} = \frac{2mr^2}{5} \\ \langle \omega^2 \rangle &= \frac{5\langle v^2 \rangle}{2r^2} \\ \langle \omega^2 \rangle &= \frac{5(0.12354)}{2(2 \times 10^{-8} \text{ m})^2} \\ \langle \omega^2 \rangle &= 7.72 \times 10^{14} \\ \omega_{rms} = \sqrt{\langle \omega^2 \rangle} &= 2.778 \times 10^7 \text{ rad/s} \\ \nu_{rms} = \frac{\omega_{rms}}{2\pi} = \sqrt{\langle \omega^2 \rangle} &= 4.42 \times 10^6 \text{ rev/s} \end{aligned}$$

which is an amazingly high rotation rate. Let's see what the inward acceleration is at the surface of a grain

$$a_{in} = \frac{v^2}{r} = \omega^2 r = 1.54 \times 10^7 \text{ m/s}^2 = 1.58 \times 10^6 g \quad (\text{where } g = 9.81 \text{ m/s}^2)$$

It seems miraculous that they can hold themselves together.

**HRK 25.3**

The relevant expression for heat transferred in a phase change is

$$Q = Lm$$

We are interested in the ice/water transition so  $L = L_f$  (fusion) and this only affects an unknown portion of the 258 g of water.

$$\begin{aligned} Q &= L_f m \\ 50.4 \text{ kJ} &= (333 \text{ kJ/kg})m \\ \Rightarrow m &= 0.151 \text{ kg of ice forms} \end{aligned}$$

The amount that is still liquid water is

$$0.258 - 0.151 = 0.107 \text{ kg}$$

### HRK 25.7

We will be using specific heat capacities  $c$  of two different materials (water:  $c_w = 4190 \text{ J/(kg K)}$ , copper:  $c_c = 387 \text{ J/(kg K)}$ ) where the general expression for heat (energy) entering/leaving an object is

$$Q = cm\Delta T$$

We also need to account for the heat that is “used up” in turning 4.7g of water into steam (so we will need the latent heat of vaporization  $Q = mL_v$  – referring to the table in your textbook we see  $L_v$  for water is  $2256 \times 10^3 \text{ J/kg}$ )

$$\begin{aligned} \text{Heat flow into water } Q_{water} &= c_w m_{water} \Delta T + m_{w \rightarrow s} L_v \\ \text{Heat flow into bowl } Q_{bowl} &= c_c m_{bowl} \Delta T \\ \text{Heat flow out of cylinder } Q_{cylinder} &= -c_c m_{cylinder} \Delta T \end{aligned}$$

We must have that the total amount of heat is conserved. Physically we know that  $Q_{water}$  and  $Q_{bowl}$  will be greater than zero (because they heat up), and  $Q_{cylinder}$  will be negative because it cools down.

$$Q_{water}^{into} + Q_{bowl}^{into} = Q_{cylinder}^{out \text{ of}}$$

Be careful with  $g$  vs.  $kg$  and  $J$  vs  $kJ$  etc. Since  $\Delta T$  is the same on the Kelvin or Celsius scale we will stick with  $^{\circ}C$

#### 25.7 (a)

$$\begin{aligned} \text{Heat flow into water } Q_{water} &= c_w m_{water} \Delta T + m_{w \rightarrow s} L_v \\ \text{Heat flow into water } Q_{water} &= (4190)(0.223)(100 - 21) + (4.7 \times 10^{-3})(2256 \times 10^3) \\ \text{Heat flow into water } Q_{water} &= 84,418 \text{ J} \end{aligned}$$

#### 25.7 (b)

$$\begin{aligned} \text{Heat flow into bowl } Q_{bowl} &= c_c m_{bowl} \Delta T \\ \text{Heat flow into bowl } Q_{bowl} &= (387)(0.146)(100 - 21) \\ \text{Heat flow into bowl } Q_{bowl} &= 4,464 \text{ J} \end{aligned}$$

## 25.7 (c)

$$\text{Heat flow out of cylinder } Q_{cylinder} = -c_c m_{cylinder} \Delta T$$

We must have that

$$\begin{aligned} 84,418 \text{ J} + 4463 \text{ J} &= -(387)(0.314)(100 - T_i) \\ 88881 &= -(121.52)(100 - T_i) \\ 731.4 &= -100 + T_i \\ 831.4^\circ\text{C} &= T_i \text{ Mistake in book} \end{aligned}$$

## HRK 25.10

When using the heat capacity  $C'$  of a particular object we have

$$Q = C' \Delta T$$

Physically we know that the heat gained by the thermometer will be equal to the heat lost by the water so

$$Q_{therm} + Q_{water} = 0$$

where

$$\begin{aligned} \text{Heat into therm } Q_{therm} &= C'_{therm} \Delta T \\ Q_{therm} &= (46.1 \text{ J/K})(44.4 - 15) \\ Q_{therm} &= 1355 \text{ J} \end{aligned}$$

and

$$\begin{aligned} \text{Heat into water } Q_{water} &= c_w m_w \Delta T \quad (\text{we know this will be negative since water cools}) \\ Q_{water} &= (4190 \text{ J/(kg K)})(0.3 \text{ kg})(44.4 - T_i) \\ Q_{water} &= 1257(44.4 - T_i) \end{aligned}$$

Solving for  $T_i$  we get

$$\begin{aligned} Q_{therm} + Q_{water} &= 0 \\ 1355 + 1257(44.4 - T_i) &= 0 \\ 57165.8 &= 1257T_i \\ T_i &= 45.5^\circ \end{aligned}$$

## HRK 25.14

We are told that the volume passing through the tube every second is

$$\text{Vol/sec} = 8.2 \text{ cm}^3/\text{s}$$

Which means that the mass of liquid passing every second is

$$\text{mass/sec} = (\rho)(\text{Vol/sec}) = (8.2 \text{ cm}^3/\text{s})(0.85 \times 10^{-3} \text{ kg/cm}^3) = 6.97 \times 10^{-3} \text{ kg/s}$$

The amount of heat entering the liquid (with specific heat capacity  $c_{liq}$ ) every second is

$$\begin{aligned} \text{Heat/sec} &= (\text{mass/sec}) c_{liq} \Delta T \\ \text{Heat/sec} &= (6.97 \times 10^{-3} \text{ kg/s})(c_{liq})(15 \text{ K}) \\ 250 \text{ J/s} &= (6.97 \times 10^{-3} \text{ kg/s})(c_{liq})(15 \text{ K}) \\ \Rightarrow c_{liq} &= 2391 \text{ J/(kg K)} \end{aligned}$$

**HRK 25.19**

This question uses the notion of linear expansion we encountered a couple of chapters ago. Recall

$$\Delta L = \alpha L \Delta T \quad \text{or} \quad L_f = L_i(1 + \alpha \Delta T) \quad (\text{equivalent})$$

The relevant lengths in this question are the diameters of the copper ring and aluminum sphere. Let us denote the coefficients of linear expansion for copper and aluminum as  $\alpha_c$  and  $\alpha_{Al}$  respectively. The sphere will drop through when  $d^{(sphere)} = d^{(ring)}$ . This happens when both objects reach the same temperature  $T_{eqm}$ . Note that the sphere will shrink as it cools down and the inner and outer diameters of the ring will both increase as it heats up

$$\begin{aligned} d_f^{(sphere)} &= d_i^{(sphere)} \left( 1 + \alpha_{Al}(T_{eqm} - T_i^{(sphere)}) \right) \\ d_f^{(ring)} &= d_i^{(ring)} \left( 1 + \alpha_c(T_{eqm} - T_i^{(ring)}) \right) \end{aligned}$$

Let us also take into account the flow of heat in this question. We have

$$Q_{ring}^{in} = Q_{sphere}^{out}$$

where

$$\begin{aligned} Q_{ring}^{in} &= m_{ring} c_c (T_{eqm} - T_i^{(ring)}) \\ Q_{sphere}^{out} &= -m_{sphere} c_{Al} (T_{eqm} - T_i^{(sphere)}) \end{aligned}$$

Since  $Q_{ring}^{in} = Q_{sphere}^{out}$  we have

$$\begin{aligned} m_{sphere} c_{Al} (T_{eqm} - T_i^{(sphere)}) &= -m_{ring} c_c (T_{eqm} - T_i^{(ring)}) \\ \Rightarrow m_{sphere} &= -m_{ring} \left( \frac{c_c}{c_{Al}} \right) \frac{(T_{eqm} - T_i^{(ring)})}{(T_{eqm} - T_i^{(sphere)})} \\ m_{sphere} &= -(21.6 \times 10^{-3}) \left( \frac{387}{900} \right) \frac{(T_{eqm} - 0)}{(T_{eqm} - 100)} \\ m_{sphere} &= -(9.3 \times 10^{-3}) \frac{(T_{eqm} - 0)}{(T_{eqm} - 100)} \end{aligned}$$

We are half-way there; now use the expression  $d_f^{(sphere)} = d_f^{(ring)}$  to finish out

$$\begin{aligned} d_i^{(sphere)} \left( 1 + \alpha_{Al}(T_{eqm} - T_i^{(sphere)}) \right) &= d_i^{(ring)} \left( 1 + \alpha_c(T_{eqm} - T_i^{(ring)}) \right) \\ (2.545333 \times 10^{-2}) \left( 1 + (17 \times 10^{-6})(T_{eqm} - 100) \right) &= (2.54 \times 10^{-2}) \left( 1 + (23 \times 10^{-6})(T_{eqm} - 0) \right) \end{aligned}$$

which if solved carefully gives

$$T_{eqm} = 34 \text{ } ^\circ\text{C}$$

and so, finally,

$$m_{sphere} = -(9.3 \times 10^{-3}) \frac{(34 - 0)}{(34 - 100)} = 4.8 \times 10^{-3} \text{ kg}$$

**HRK 25.22**

Using molar heat capacity,  $C$ , the amount of heat transferred looks like

$$\begin{aligned} Q &= nC\Delta T \quad \text{if } C \text{ constant} \\ \text{or } Q &= \int_{T_i}^{T_f} nC(T) dt \quad \text{if } C = C(T) \end{aligned}$$

Our case is the latter so

$$\begin{aligned}
 Q &= n \int_{50}^{90} (0.318T - 0.00109T^2 - 0.628) dt \\
 Q &= n \left[ 0.318 \frac{T^2}{2} - 0.00109 \frac{T^3}{3} - 0.628T \right]_{50}^{90} \\
 Q &= n(645.8)
 \end{aligned}$$

The number of moles is given by

$$n = \frac{316 \text{ g}}{107.8 \text{ g/mol}} = 2.93 \text{ mol}$$

so that

$$Q = 1893 \text{ J}$$

### HRK 25.25

The heat transferred in a constant-pressure process is

$$Q = nC_p\Delta T$$

where  $C_p$  is the molar heat capacity at a constant temperature. Table 3 give the value for  $O_2$  gas,  $C_p = 29.4 \text{ J/(mol K)}$ . To find  $\Delta T$  we use

$$\begin{aligned}
 \frac{V_1}{T_1} &= \frac{V_2}{T_2} && \text{constant pressure} \\
 \frac{V_1}{T_1} &= \frac{2V_1}{T_2} \\
 \Rightarrow T_2 &= 2T_1 \\
 \Rightarrow \Delta T &= 2T_1 - T_1 = 284 \text{ K}
 \end{aligned}$$

$$Q = nC_p\Delta T$$

$$Q = (1.35)(29.4)(284) = 11,272 \text{ J}$$